

Water-soluble or water-dispersible (co)polymers of hydroxyalkyl (meth)acrylates, a process for their preparation, and their use as coating agent, binder and/or film-forming excipient in  
5 pharmaceutical dosage forms

The present invention relates to water-soluble or water-dispersible copolymers of hydroxyalkyl (meth)acrylates, a process for their preparation, and their use as coating agent,  
10 binder and/or film-forming excipient in pharmaceutical dosage forms.

Solid pharmaceutical dosage forms such as tablets, capsules, pellets, granules, crystals etc. are coated, i.e. provided with a  
15 film coating, for a wide variety of reasons. It is possible in this way, for example, to mask an unpleasant odor or taste, and improve the swallowability. The stability of the active ingredient can be increased by the coating, since less water vapor and oxygen reaches the interior of the tablets. The dosage  
20 forms have a better appearance and can be distinguished better by incorporating dyes. In addition, in particular the rate of release of the active ingredient can be adjusted by the film coating.

25 A distinction is made in general between instant release forms and sustained or slow release forms.

In the case of instant release forms, the disintegration of the tablet and the release of the active ingredient from the dosage  
30 form should, where possible, be unaffected by the coating, for which reason the film coating must dissolve rapidly in gastric fluid. In addition, it must have good film properties. The tensile strength and the ultimate elongation ought to be high so that the film coating withstands mechanical effects like those  
35 occurring during pharmaceutical processing - especially packaging - and during transport and storage.

A product which is frequently employed for coating instant release tablets is hydroxypropylmethylcellulose (HPMC).  
40 Hydroxypropylmethylcellulose shows a steep rise in viscosity with increasing concentration in aqueous solution. Hydroxypropylcellulose (HPC) also shows a similar behavior.

Since the film former solution must be finely atomized for  
45 coating tablets, and the drops which are formed must thoroughly wet the surface of the tablets, and moreover spread well, the viscosity must not exceed a certain limit (between 150 and 250

mPas), which depends on the type of spray nozzle and the equipment. It is therefore possible in the case of HPMC to employ only relatively low film former concentrations.

- 5 The recommendation given in the literature for the concentration of Pharmacoat® 606 (from Shin-etsu) is 5 to 7% by weight (Pharmaceutical Coating Technology, edited by Graham Cole, Taylor and Francis Ltd. 1995 and manufacturers' technical data sheets). These low spray concentrations result in a relatively long  
10 processing time and thus high costs.

- In addition, hydroxypropylmethylcellulose has other disadvantages, inter alia in the wetting characteristics, in the adhesiveness on the tablet surface, in the pigment binding  
15 capacity, in the mechanical properties of the films, in the hygroscopicity and in the permeability for water vapor and oxygen, in the rate of solution and in the difference in disintegration time between film-coated tablet and core.
- 20 The low elasticity of the films of hydroxypropylmethylcellulose frequently lead to the film-coated tablets splitting open on storage in moist conditions, as a consequence of the swelling of the core. Even the use of plasticizers results in negligible improvements in this problem. On the contrary, it may lead to  
25 tacky films and, through migration, to changes in the tablet properties.

- Binders are employed in pharmaceutical dosage forms in order to increase the processability and the mechanical strength. They are  
30 normally employed in tablets, granules and pellets and result in improved flowability, greater hardness and less friability.

- The binders used at present such as maltodextrin or polyvinylpyrrolidone frequently do not result in satisfactory  
35 hardnesses and friabilities. Other binders such as starch paste and hydroxypropylmethylcellulose (HPMC) can be employed only in low concentrations because of their high viscosity.

- In addition, film-forming excipients are employed in solutions  
40 and sprays which are applied to the skin or mucous membrane or else introduced systemically into the body. Examples thereof are preparations for wound treatment and spray-on dressings, but also preparations for application to intact skin or mucous membrane.
- In this case, the skin is protected by a film, and the active  
45 ingredients can penetrate into or through the skin.

Great flexibility is necessary for transdermal therapeutic systems and for wound plasters, just as for the abovementioned dosage forms, but the products available at present do not have this. The use of possible plasticizers to achieve the necessary flexibility is undesirable for toxicological and pharmacological reasons.

GB 1 278 813 describes acrylate emulsion polymers which are distinguished by high water resistance compared with conventional soap dispersions, which makes them unsuitable for use in instant release tablets.

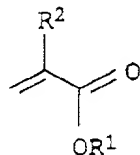
DE 31 11 602 describes emulsion polymers which are stabilized by polyvinyl alcohol and comprise at least 60% by weight (meth)acrylate and/or styrene units. They are used as binders for emulsion paints and adhesives.

DE-A 196 29 948 discloses dispersions in which styrene is an obligatory constituent and which are used as starting materials in building materials.

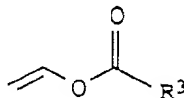
It is an object of the present invention to provide water-soluble or water-dispersible polymers as coating agents, binders and/or film-forming excipients in pharmaceutical dosage forms, in particular for instant release forms, which do not have the abovementioned disadvantages.

We have found that this object is achieved by water-soluble or water-dispersible copolymers which are obtainable by free-radical polymerization, preferably emulsion polymerization, of

- a) 80 to 20% by weight of hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylate and, where appropriate, one or more compounds of the formula (A) or (B)



(A)



(B)

with R<sup>1</sup> = H, C<sub>1</sub>-C<sub>6</sub>-alkyl,  
R<sup>2</sup> = H, CH<sub>3</sub>  
R<sup>3</sup> = C<sub>1</sub>-C<sub>24</sub>-alkyl

4

or mixtures thereof

in the presence of

- 5      b) 20 to 80% by weight of polyvinyl alcohol (PVA) and
- c) where appropriate 0 to 20% by weight of other polymerizable compounds (C).
- 10 The invention further relates to a process for preparing the copolymers by free-radical polymerization, preferably emulsion polymerization, in an aqueous or nonaqueous but water-miscible solvent or in mixed nonaqueous/aqueous solvents. Preparation in water as solvent or dispersant is preferred.
- 15      Examples of suitable nonaqueous solvents are alcohols such as methanol, ethanol, n-propanol and isopropanol, and glycols such as ethylene glycol and glycerol.
- 20 The hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylate preferably employed is hydroxymethyl methacrylate, hydroxyethyl methacrylate, hydroxypropyl methacrylate, hydroxybutyl methacrylate or hydroxypentyl methacrylate, particularly preferably hydroxyethyl methacrylate. The compounds of the formula (A) which are
- 25 preferably employed are C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylates, in particular methyl methacrylate, ethyl acrylate and methyl acrylate or mixtures thereof. The compounds of the formula B employed are C<sub>3</sub>-C<sub>24</sub> vinyl esters, in particular vinyl acetate. Compounds of the formula A are preferred to compounds of the formula (B).
- 30      Suitable and preferred compounds (C) are: acrylic and methacrylic acids. Further compounds (C) are crotonic acid, mono(C<sub>1</sub>-C<sub>8</sub>)-alkyl maleates, maleic acid, fumaric acid, itaconic acid, (meth)acrylonitrile, ethylenically unsaturated di(C<sub>1</sub>-C<sub>22</sub>)-alkyl
- 35 dicarboxylates, preferably butyl maleate, ethylenically unsaturated sulfonic acids or sulfonic acid derivatives such as vinylsulfonic acid or the alkali metal salts thereof, acyclic N-vinylcarboxamides and N-vinyl lactams such as vinylpyrrolidone.
- 40 It is also possible for multiply ethylenically unsaturated copolymerizable compounds which can act as crosslinkers to be present, preferably from the group of divinylbenzene, diallyl phthalate, butanediol diacrylate, butanediol dimethacrylate. Further suitable crosslinking monomers are mentioned, for
- 45 example, in DE 197 12 247 A1, page 5. However, the content of compounds (C) is preferably 0% by weight.

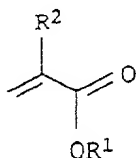
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A preferred embodiment of the invention comprises water-soluble or water-dispersible copolymers which are obtainable by free-radical polymerization, preferably emulsion polymerization, of

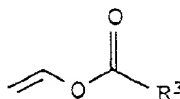
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- a) 80 to 20% by weight of hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylate and, where appropriate, one or more compounds of the formula (A) or (B)

10



(A)



(B)

15

with R<sup>1</sup> = H, C<sub>1</sub>-C<sub>6</sub>-alkyl,

R<sup>2</sup> = H, CH<sub>3</sub>

R<sup>3</sup> = C<sub>1</sub>-C<sub>24</sub>-alkyl

20

or mixtures thereof

in the presence of

25

- b) 20 to 80% by weight of polyvinyl alcohol (PVA) and

- c) where appropriate 0 to 20% by weight of other polymerizable compounds (C), where the content of hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylate in % by weight is at least once, preferably

30

twice, in particular three times, as large as the content of compounds of the formula (A) or (B) in % by weight.

Suitable and preferred polyvinyl alcohols (PVA) are partially hydrolyzed, as well as completely hydrolyzed, (cold)

35

water-soluble PVA with molecular weights between about 2000 and about 250,000, in particular about 10,000 to 100,000, as are obtained by alcoholysis or hydrolysis of polyvinyl esters, preferably of polyvinyl acetates. Preferred PVA have a degree of hydrolysis of from 65 to 99%, particularly preferably of from 80

40

to 90%.

The polymerization preferably takes place in the presence of from 20 to 80% by weight, preferably of from 25 to 60% by weight, in particular of from 30 to 55% by weight, of polyvinyl alcohol. The

45

"remainder" up to 100% by weight is in each case constituted by

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the compounds hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylate, A and/or B or (C).

If one or more compounds of the formula A or B are employed in addition to hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylates, the content of hydroxy-C<sub>1</sub>-C<sub>6</sub>-alkyl (meth)acrylates in % by weight is at least once, preferably at least twice, particularly preferably at least three times, as large as the content of compounds of the formula (A) or (B) in % by weight.

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The polymers can be prepared by polymerizing the monomers of the formula A and/or B and/or C in the presence of the PVA both with the aid of free-radical initiators and by the action of high-energy radiation, which is intended to be understood to include the action of high-energy electrons.

The emulsion polymerization is preferably carried out at temperatures of from 60 to 100°C.

20 The emulsion polymerization is initiated by employing free-radical initiators. The amounts of initiator or initiator mixtures used are between 0.01 and 10% by weight, preferably between 0.3 and 5% by weight, based on monomer employed.

25 Depending on the nature of the solvent used, both organic and inorganic peroxides or azo initiators are suitable, such as azobisisobutyronitrile, azobis(2-amidinopropane) dihydrochloride or 2,2'-azobis(2-methylbutyronitrile).

30 Examples of peroxide initiators are dibenzoyl peroxide, diacetyl peroxide, succinyl peroxide, tert-butyl perpivalate, tert-butyl per-2-ethylhexanoate, tert-butyl permaleate, bis(tert-butylperoxy)cyclohexane, tert-butylperoxy isopropyl carbonate, tert-butyl peracetate,

35 2,2-bis(tert-butylperoxy)butane, dicumyl peroxide, di-tert-amyl peroxide, di-tert-butyl peroxide, p-menthane hydroperoxide, pinane hydroperoxide, cumene hydroperoxide, tert-butyl hydroperoxide, hydrogen peroxide and mixtures of said initiators. Said initiators can also be used in combination with redox

40 components such as ascorbic acid.

Alkali metal or ammonium persulfates are particularly suitable as initiator.

45 The free-radical emulsion polymerization preferably takes place in water in the presence of polyvinyl alcohol and in the presence of free-radical polymerization initiators, where appropriate

- emulsifiers, where appropriate other protective colloids, where appropriate molecular weight regulators, where appropriate buffer systems, and where appropriate subsequent pH adjustment using bases or acids. The copolymers are obtained as aqueous
- 5 dispersions or aqueous solutions with a viscosity of less than 500 mPas, preferably less than 250 mPas, particularly preferably less than 150 mPas, or, after removal of the water content, as water-dispersible or water-soluble powders.
- 10 Suitable protective colloids besides PVA are water-soluble cellulose derivatives, preferably from the group of hydroxyethylcellulose, carboxymethylcellulose, carboxymethylhydroxyethylcellulose, methylhydroxyethylcellulose, or water-soluble (co)polymers composed of N-vinylamide compounds
- 15 of N-vinyl lactam compounds, preferably polyvinylpyrrolidone (PVP), or water-soluble polymeric, copolymeric or block-copolymeric polyalkylene oxides, preferably of ethylene oxide and/or propylene oxide.
- 20 Suitable molecular weight regulators are hydrosulfide compounds such as alkyl mercaptans, e.g. n-dodecyl mercaptan, tert-dodecyl mercaptan, thioglycolic acid and its esters, mercaptoalkanols such as mercaptoethanol. Other suitable regulators are mentioned, for example, in DE 197 12 247 A1, page 4. The amount required of
- 25 the molecular weight regulators is in the range from 0 to 5% by weight based on the amount of (co)monomers to be polymerized, in particular 0.05 to 2% by weight, particularly preferably 0.1 to 1.5% by weight.
- 30 Examples of emulsifiers used are ionic or nonionic surfactants, whose HLB is normally in the range from 3 to 13. Concerning the definition of the HLB, reference is made to the publication by W.C. Griffin, J. Soc. Cosmetic Chem., Volume 5, 249 (1954).
- 35 The type of emulsifier and the mode of addition of the emulsifier influence the polymerization: it is possible in this connection to observe differences in the particle size, particle size distribution, stability of the copolymer dispersion and the extent of the grafting reactions, for example depending on
- 40 whether the emulsifier is present in the initial charge or is metered in during the copolymerization. Examples of preferred anionic emulsifiers for preparing anionic emulsion copolymers are surface-active alkyl sulfates, alkylsulfonates, alkylaryl sulfates, alkylarylsulfonates, alkali metal and/or ammonium salts
- 45 of alkyl or alkylaryl monoglycol or polyglycol ether sulfates. Preferred nonionic emulsifiers are, for example, ethoxylated fatty alcohols or ethoxylated alkylphenols. Particularly

preferably used according to the invention is sodium lauryl sulfate, also in combination with polysorbate 80.

The amount of surfactants is 0.05 to 10% by weight, preferably  
5 0.1 to 5% by weight, based on the polymer.

In the case of emulsion polymerization, it may be of crucial importance whether the monomer is metered in as such or as an aqueous emulsion. The aqueous emulsion of the monomers usually  
10 contains water, anionic and/or nonionic emulsifiers and/or protective colloids such as polyvinyl alcohol and, where appropriate, other protective colloids and, where appropriate, regulators. The monomer or a monomer mixture or the monomer emulsion is introduced together with the initiator, which is  
15 generally present in solution, into a stirred reactor at the polymerization temperature (batch process) or, where appropriate, metered continuously or in a plurality of consecutive stages into the polymerization reactor (feed process). It is usual in the feed process for the reactor to be charged before starting the  
20 actual polymerization with, besides water (in order to make stirring of the reactor possible), also partial quantities, rarely the entire amount intended for the polymerization, of the starting materials such as emulsifiers, protective colloids, monomers, regulators etc. or partial quantities of the feeds  
25 (generally monomer feed or emulsion feed and initiator feed).

It must also be taken into account that copolymerization of each of the comonomers used must be possible in principle and that it also in fact takes place. In the simplest case, this can be  
30 estimated with the assistance of the copolymerization parameters or the Q and e values (cf., for example, B. Brandrup, Immergut, Polymer Handbook, 2<sup>nd</sup> ed. (1975), John Wiley & Sons, New York).

It is thus possible where appropriate for a copolymerization in  
35 some circumstances to be made feasible by having one or more monomer components present in the initial charge and metering in the remaining monomer or the remaining monomer mixture only during the polymerization.

40 The solids content of the resulting aqueous polymer dispersions or solutions is usually 10 to 70% by weight, preferably 20 to 60% by weight, particularly preferably 25 to 40% by weight.

The polymer dispersions or solutions can be converted into powder  
45 form by various drying processes such as, for example, spray drying, fluidized spray drying, drum drying or freeze drying. Spray drying is preferably employed as drying process owing to





They improve the solubility and rate of dissolution of medicinal substances of low solubility in water by interacting with them, whereby the absorbability and bioavailability of the medicinal substances are improved. This advantageous effect is evident, for example, with dosage forms in which the active ingredient is not present in solution, such as, for example, tablets, granules, suspensions etc.

The polymers used according to the invention can, where appropriate also in combination with other excipients, be processed together with active ingredients to give polymer/active ingredient melts which either undergo extrusion and calendering to give drug products or, after the extrusion, are converted into granules or powders and only then processed to drug forms, for example compressed to tablets. In these cases, the copolymers introduce the properties detailed above into the dosage form.

The polymers of the invention are able to perform the following functions outstandingly in various pharmaceutical dosage forms:

Dispersing aid, suspending aid, wetting agent, solubilizer for medicinal substances of low solubility, emulsifier, crystallization inhibitor, anticaking aid, protective colloid, spreading aid, viscosity regulator, excipient for producing solid solutions with medicinal substances, excipient for adjusting release of active ingredient.

When used to produced suppositories and pessaries, the polymers on the one hand ensure the flexibility of the dosage form, and on the other hand promote the disintegration and the dissolution of active ingredient, and they coat the mucous membrane with an active ingredient-containing film which enhances absorption. As the comparison of the viscosities of the polymers of the invention (Example 1, viscosity 77 mPas) with corresponding solutions of hydroxymethylpropylcellulose (Pharmacoat 606) (Example 1, viscosity 2000 mPas) shows, the polymers of the invention have a considerably lower viscosity.

It is thus possible to employ more concentrated polymer preparations when coating tablets with the polymer dispersions, as well as for binder applications, which allows the processes to be made considerably more cost-effective and time-saving.

The dissolution or redispersion of the polymers in powder or granule form to give aqueous dispersions or solutions takes place considerably more quickly than with other film formers or binders, because the polymers of the invention are thoroughly

wetted by water and show little agglomeration and a very high dissolution rate.

Gastric fluid-soluble tablets coated with the polymers show a  
5 disintegration time which is only slightly longer than that for the core, i.e. the film coating dissolves very rapidly in simulated gastric fluid.

In addition, the mechanical strength of the tablets is increased  
10 very much more when the polymers are used according to the invention than with hydroxypropylmethylcellulose.

Tablets swell to different extents depending on the excipients and active ingredients used, the storage time and the storage  
15 conditions, such as temperature and humidity. A rigid film coating develops cracks when the core swells. The elasticity of film formers is therefore an important quantity. The copolymers of the invention have an exceptionally high flexibility and elasticity. Thus, the ultimate elongation may be up to 300%. No  
20 crack formation is therefore to be expected, even if the core swells greatly.

The polymers can be applied in pure form or else together with conventional excipients to the active ingredient-containing core.  
25 Examples of conventional excipients are colored pigments for coloring, white pigments such as titanium dioxide to increase the hiding power, talc and silica as non-stick agents, polyethylene glycols, glycerol, propylene glycol, triacetin, triethyl citrate as plasticizer and various surface-active substances such as  
30 sodium lauryl sulfate, polysorbate 80, Pluronic und Cremophors to improve the wetting characteristics. The substances mentioned by way of example do not represent a restriction. It is possible to use all additives known to be suitable for gastric fluid-soluble film coatings.

35 It is also possible to combine the polymers used according to the invention with other film formers or polymers in the ratio from 1:9 to 9:1.

40 Examples of polymers which can be employed for this purpose are the following:

Polyvinylpyrrolidone, polyvinylpyrrolidone copolymers, water-soluble cellulose derivatives such as  
45 hydroxypropylcellulose, hydroxypropylmethylcellulose, methylcellulose, hydroxyethylcellulose, acrylate and methacrylate

copolymers, polyvinyl alcohols, polyethylene glycols, polyethylene oxide/polypropylene oxide block copolymers.

The coating processes which can be used are the conventional  
5 processes such as coating in a fluidized bed or in a horizontal drum coater, the drip-coating process and the pan-coating process. Besides the use for tablets, the polymers of the invention can also be employed for coating other pharmaceutical preparations such as granules, pellets, crystals or capsules. The  
10 novel coating agents are applied in a conventional manner in a thickness of from 5 to 200  $\mu\text{m}$ , preferably 10 to 100  $\mu\text{m}$ .

In their use as binder, a distinction is made between wet and dry binders depending on the processing method. The latter are used  
15 inter alia for direct tableting and for dry granulation or compaction. In these cases, the binder is mixed with the active ingredient and, where appropriate, other excipients and then directly tableted, or granulated or compacted.

20 In contrast thereto, in wet granulation the active ingredient/excipient mixture is moistened with a solution of the binder in water or an organic solvent, and the moist composition is passed through a sieve and then dried. The moistening and drying may moreover take place in parallel, such as, for example,  
25 in fluidized-bed granulation.

For optimal processing, the binder should have low viscosity in solution because viscous solutions lead to inhomogeneous granules.

30 A binder should lead to uniform, hard, nonfriable granules or tablets. The hardness is particularly important for tablets because many active ingredients are difficult to compress and thus afford tablets with inadequate mechanical stability.

35 In addition, the binder should have a negligible adverse effect on the disintegration of the drug forms and the rate of release of the active ingredients.

40 The most commonly used binders are, for example, polyvinylpyrrolidone, vinyl acetate / vinylpyrrolidone copolymers, gelatin, starch pastes, maltodextrins, hydroxyalkylated and carboxyalkylated cellulose derivatives, such as hydroxypropylmethylcellulose, methylcellulose, sodium  
45 carboxymethylcellulose, natural gum types such as gum arabic, pectin or alginate.



14

Feed 2                      5.0 g      of 7% strength aqueous sodium  
persulfate solution

Feed 3                      30.0 g      of 7% strength aqueous sodium  
persulfate solution  
5                              55.0 g      of deionized water

Apparatus: 2 l pilot stirred apparatus, oil bath, anchor stirrer,  
process control system for feeds

10 The apparatus is flushed with nitrogen

#### Procedure

The precharge was heated to an internal temperature of 80°C. At  
about 75°C, feed 2 was metered in and polymerized for 15 minutes.

15 Feed 1 was added in 1.5 h, and feed 3 was added simultaneously in  
10 minutes. Polymerization was continued at 80°C for 3 h after  
completion of feed 1. The mixture was then cooled and filtered  
through 120 mm.

20 Solids content                      28.9% by weight  
Average particle size                  325 nm  
Coagulum                              0.1 g

Viscosity (20% solution)              77 mPas

25

Film properties (54% R. H., 23°C)  
Ultimate elongation                    43 %  
Tear strength                          45 N/mm<sup>2</sup>

30 Comparison Pharmacoat® 606 (from Shin-etsu)  
Viscosity (20% solution)              2000 mPas

Film properties (54% R.H., 23°C)  
Ultimate elongation                    17%

35 Tear strength                        58 N/mm<sup>2</sup>

#### Use Example

Production of propranolol HCl film-coated tablets (gastric  
40 fluid-soluble coating)

A film coating of the following composition:

45

15

5	Polymer from Example 1 Polyvinyl alcohol / hydroxyethyl methacrylate / methyl methacrylate	12.0% by weight
	Sicovit® rot (from BASF Aktiengesellschaft)	1.5% by weight
	Titanium dioxide BN 56 (from Kronos)	3.0% by weight
	Talcum powder (from Riedel de Haen)	4.5% by weight
10	Water	79.0% by weight

was sprayed onto 9 mm biconvex tablet cores containing 40 mg of propranolol HCl (from Knoll AG), 195.0 mg of Ludipress® (from BASF Aktiengesellschaft), 12.50 mg of Kollidon® VA 64 (from BASF Aktiengesellschaft) and 2.50 mg of magnesium stearate in a horizontal drum coater (Accela-Cota 24", from Manesty).

The spray dispersion was prepared by redispersing the spray-dried polymer from Example 1 in water by stirring, adding Sicovit® rot, titanium dioxide and talcum and then homogenizing in a corundum disk mill. 1090 g (including an overage of 10% for spray losses) were applied to 5000 g of cores at an inlet air temperature of 55°C and a spraying rate of 31 g/min using a spraying nozzle with a width of 1.0 mm and a spraying pressure of 1.8 bar. The spraying was followed by drying at 55°C for 5 min.

Smooth, glossy, red film-coated tablets were obtained with the following properties:

Appearance: very smooth surface,  
nicely formed imprint

Disintegration

(simulated gastric fluid): 5 min. 13 s.

Disintegration time difference

(coated tablet-core): 55 s.

Hardness: 94 N

Hardness difference

(Coated tablet-core): 24 N